

AIR-HEATING SET CONTROL VIA DIRECT SEARCH METHOD AND STRUCTURED SINGULAR VALUE

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ABSTRACT

The contribution describes an application of the algebraic μ -synthesis to the control of a real plant with a nonlinear characteristic. The controller design is considered as a problem of minimization of the peak of the structured singular value denoted μ . The algebraic approach consists of the pole placement principle based on the polynomial Diophantine equations and Differential Migration procedure used for optimization. The results are compared with other controllers designed via the D - K iteration, synthesis in the ring of proper and stable functions and the Naslin method.

Keywords: robust control, evolutionary computation, genetic algorithms, algebraic approaches, structured singular value, PID control, time delay systems

1. INTRODUCTION

Intensive research activity performed in the robust control theory during the recent years has brought new methods considering the parametric, dynamic and mixed structured uncertainties. Some of the methods are based on the H_∞ approach in the ring of stable and proper transfer functions denoted R_{PS} . These methods provide a measure that indicates the robustness of designed controller. However, this measure evaluates only the robust stability. On the other hand, methods based on the Zames' small gain theorem (Zames 1981) yield both the robust stability and performance conditions. One of them is the structured singular value denoted μ (Doyle 1982, Packard and Doyle 1993) treating the robust stability and performance objectives simultaneously. Two methods for the μ -synthesis were derived: the D - K iteration (Doyle 1985) and μ - K iteration (Lin et al. 1993). The D - K iteration yields a suboptimal controller minimizing the peak of the upper bound for μ -function. However, the controller has usually a high order transfer function due to the scaling matrices D , D^{-1} and for further application it is simplified via some kind of approximation. If the simplification is too substantial it can cause degradation of the frequency properties of the controller and the whole feedback loop. In some cases, the scaling matrices cannot be approximated with the desired precision and the resulting controller can be far from the optimality. Moreover, the state-space formulae

for the H_∞ suboptimal controller require the stability of the performance weighting function (Doyle et al. 1989). These problems can be resolved using the algebraic μ -synthesis (Dłapa et al. 2009, Dłapa and Prokop 2010) presented in this contribution, which overcomes both the approximation of the scaling matrices D , D^{-1} and the impossibility of integrating behaviour of the performance weighting function. In this method the controller is designed through the algebraic pole placement principle applied to the nominal plant and the position of the nominal closed-loop poles is tuned through an evolutionary algorithm with evaluation of the upper bound for μ . The problem of instability of performance weighting function is treated by setting the nominal closed-loop poles to the real axis in the left half-plane.

2. PLANT DESCRIPTION AND IDENTIFICATION

The control of heating systems has been an important field in the control theory for decades. There is a number of applications of temperature control involving nonlinear and time-delay systems present in the electrical and heating industry as well as in technology processes (e.g. Fiser 2002 or Liu 2003).

The problem of nonlinear control can be treated by adaptation to parameters changes or by using a robust or nonlinear controller. The usage of the adaptive control is limited by recursive identification, which has not satisfactory results when the input to the controller is subject to noise or if there are other factors, such as time delay or external disturbances causing inaccuracy of measured signals. The algebraic μ -synthesis presented in this contribution is more versatile than common methods for the robust control and can consider the effects of noise, nonlinearity and time delay as well as the influence of external disturbances. However, the usage of this method is limited to the models fitting in the linear fractional transformation (LFT) framework. In order to describe nonlinearity of controlled plant the parametric uncertainty is used and transformed to LFT interconnection which does not increase conservatism of the plant model.

The air-heating set considered in this contribution has three input and seven measured quantities. The input signals are the voltage on bulb and the main and

adjacent fan. The circuit was controlled by a standard IBM PC computer, which communicates via serial link (RS232) with the CTRL unit (see Figure 1). The CTRL unit converts the digital data to unified analogue signals. In the transformation and unification unit the unified analogue signals are transformed to the voltage on a particular actuator. Similarly, the measured signals are transformed to the unified voltage 0-10 V (Table 1).

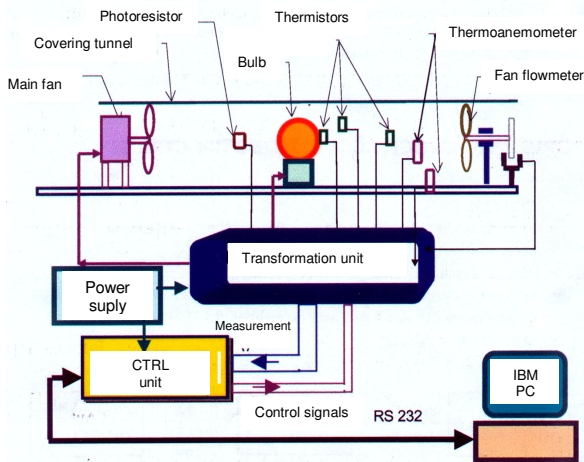


Figure 1: Plant Scheme

Table 1: Input and Output Channels of CTRL Unit

Inputs	Sensor	Outputs	Actuator
y1	sensor of bulb radiance	u1	voltage of bulb
y2	sensor of temperature near bulb T ₂	u2	voltage of main fan (speed control)
y3	temperature of envelope of the bulb T ₃	u3	voltage of adjacent fan (speed control)
y4	temperature at output of tunnel T ₄		
y6	thermoanemometer TA ₆		
y7	fan flowmeter		

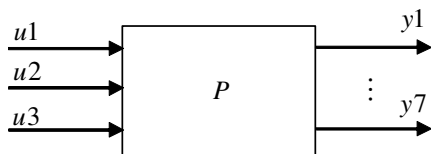


Figure 2: Inputs and Outputs of Plant

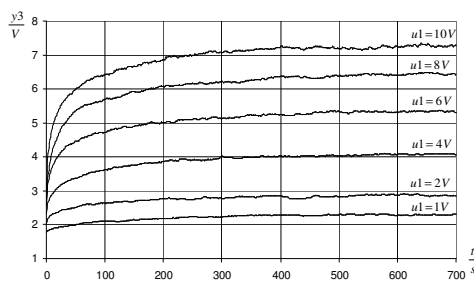


Figure 3: Step Responses of Bulb Temperature

The step responses of the measured quantity y3 (bulb temperature) for the step of u1 (bulb voltage) and constant speed of the main fan (u2 = 2V) are depicted in Figure 3. It is clear from the figure that the step responses have a nonlinear behaviour. The plant acts as if it has a short time constant at the beginning and it

slows down at the end of history. Hence it should be taken into account that the time constant will vary in a large range. It follows from the steady-state load characteristic that the gain varies in the range of 0.42 to 0.54. The family of transfer function from u1 to y3 at u2 = 2V is:

$$\mathbf{P}_{31} = \left\{ \frac{k}{Ts+1} : k \in (0.42; 0.54), T \in (5; 20) \right\} \quad (1)$$

This means that both the numerator and denominator in (1) are interval polynomials.

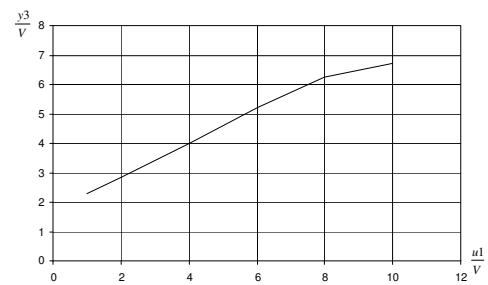


Figure 4: Steady-State Load Characteristic

3. OUTLINE OF POLE PLACEMENT DESIGN

The pole placement principle is one of the well-known methods for the controller design (e.g. Kucera 1991, Kucera 1993, Prokop and Corriou 1997, Prokop et al. 1992, Vidyasagar 1985) which is simple for derivation and tuning. Consider a simple feedback loop (1DOF) structure depicted in Figure 5 with two external inputs – the reference w and disturbance v, respectively. The output and tracking error is according to Figure 5 in the form

$$y(s) = \frac{bq}{d} w(s) + \frac{cfp}{d} v(s) \quad (2)$$

$$e(s) = w(s) - y(s) = \frac{afp}{d} \cdot \frac{h_w}{f_w} - \frac{cfp}{d} \cdot \frac{h_v}{f_v} \quad (3)$$

where

$$afp + bq = d \quad (4)$$

is the characteristic polynomial of the closed-loop system in Figure 5.

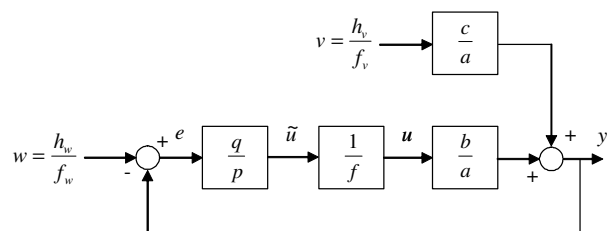


Figure 5: Structure of 1DOF system

It can be proven that the asymptotic tracking of the reference is achieved if and only if the polynomial pfa is divisible by the unstable part of f_w and v is rejected if pfa is divisible by the unstable part of f_v so that the result is a finite polynomial. As a consequence, the polynomials p, q are the solutions to Diophantine equation (4). It is also desirable that the transfer function $\frac{q}{fp}$ is proper. Analysis of the polynomial degrees in (4) for the most frequent case $f_w = f = s$ (the stepwise reference) gives

$$\deg d = 2 \deg a \quad (5)$$

A standard choice for the polynomial d is

$$d(s) = \prod_{i=1}^{\deg d} (s + \alpha_i) \quad (6)$$

where $\alpha_i > 0$ are the tuning parameters of the controller and d is a stable polynomial which ensures the internal stability of the nominal system.

With respect to (1) a nominal plant transfer function can be expressed by the transfer function

$$P(s) = \frac{b(s)}{a(s)} = \frac{b_0}{s + a_0} \quad (7)$$

and

$$w = \frac{h_w}{f_w} = \frac{1}{s} \quad (8)$$

$$v = \frac{h_v}{f_v} = \frac{1}{s} \quad (9)$$

Then equation (4) has the form

$$(s + a_0)s + b_0(q_1s + q_0) = s^2 + d_1s + d_0 \quad (10)$$

and by simple equating the coefficients at the like power of s at the left and right of (10) it can be obtained

$$\begin{aligned} q_1 &= (d_1 - a_0)/b_0 \\ q_0 &= d_0/b_0 \end{aligned} \quad (11)$$

Then the resulting controller is proper and has the traditional PI structure in the form

$$Q = \frac{q_1s + q_0}{s} \quad (12)$$

4. PRINCIPLES OF μ -SYNTHESIS

The parametric uncertainty in \tilde{P}_{31} can be treated via the LFT framework by using the additive and quotient uncertainty. Define the nominal plant

$$P_{31} = \frac{0.48}{12.5s + 1} \quad (13)$$

Plant family \tilde{P}_{31} is then equivalent to

$$\begin{aligned} \tilde{P}_{31}(s, \Delta) &= \frac{0.48 + 0.06\delta_2}{12.5s + 1} \frac{1}{1 + \frac{7.5\delta_3s}{12.5s + 1}} \\ \Delta &= \begin{bmatrix} \delta_2 & 0 \\ 0 & \delta_3 \end{bmatrix}, \delta_2, \delta_3 \in (-1; +1) \end{aligned} \quad (14)$$

Let

$$W_2(s) = \frac{0.06}{12.5s + 1}, W_3(s) = \frac{7.5s}{12.5s + 1} \quad (15)$$

then

$$\tilde{P}_{31}(s, \Delta) = (P_{31} + \delta_2 W_2) \frac{1}{1 + \delta_3 W_3} \quad (16)$$

Expression (16) is represented by the LFT interconnection depicted in Figure 6.

The LFT interconnection for the μ -synthesis which considers the performance objectives and noise suppression is in Figure 7.

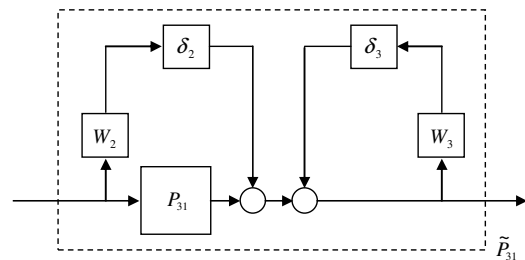


Figure 6: Structure of 1DOF system

Weight W_1 for the performance evaluation was chosen as

$$W_1(s) = \frac{0.01s + 1}{s + 0.0001} 0.09 \text{ and } \frac{0.01s + 1}{s} 0.09 \quad (17)$$

for the D - K iteration and algebraic approach, respectively.

The weight for the D - K iteration cannot have integrating behaviour because all weights must be stable. Moreover, it causes uncontrollable states in the closed-loop system. The instability and uncontrollability of the closed-loop in Figure 7 does not make the resulting feedback loop unstable if there is a guarantee that the poles of the nominal feedback loop are in the left half plane. Controllability is a necessary condition for using the state space formulae giving the H_∞ suboptimal controller (Doyle et al. 1989) as well as stability of all weighting functions. Thus it is impossible

5. CONTROL OF AIR-HEATING PLANT

Experimental studies have been carried out in order to assess the performance of the algebraic μ -synthesis method. The set-point temperature profile provides a reference which comprises 800 iterations. It consists of an initial soak at 3V for 480 iterations followed by a step to 4V which is held constant for 300 iterations. Sampling period is 1 s and adjacent fan voltage is kept zero for all experiments.

The experimental trials are aimed at evaluating the performance of the PI controller obtained via the algebraic μ -synthesis against the D - K iteration, synthesis in the R_{PS} with the poles in one point and the Naslin method.

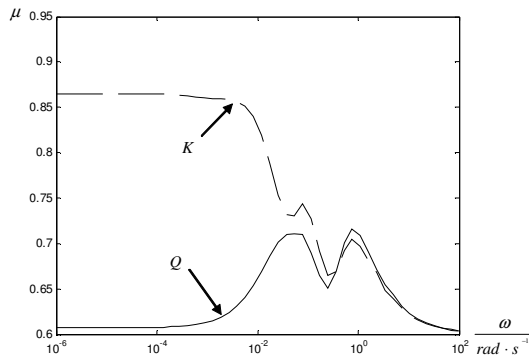


Figure 9: μ -Plot for D - K Iteration (dashed) and Algebraic μ -Synthesis (solid)

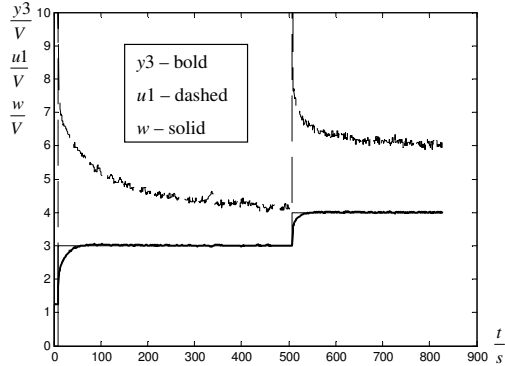


Figure 10: Control of Real Plant for Algebraic Approach

Performance indices. In order to draw comparisons between different control schemes an index or measure of performance is required. The measure of effectiveness which is adopted consists of three factors, these being the amount of energy, the variance of the controlled actuators and the accuracy of set-point tracking. This may be expressed as

$$\epsilon_1 = \frac{\sum u(t)}{\rho} \quad (26)$$

where ρ is the number of iterations.

In cases where there is an increased variance in the control signals to the actuator this can lead to

correspondingly increased costs due to maintenance and down time due to failure. The variance of the controlled actuator may be expressed in the form

$$\epsilon_2 = \sum [u(t) - \epsilon_1]^2 \quad (27)$$

The resulting controller quality arising from control action may be expressed in terms of the accuracy of set-point tracking. Using the integral of absolute error the deviation of the system response $y(t)$ from the set-point $r(t)$ is given as

$$\epsilon_3 = \sum |y(t) - r(t)| \quad (28)$$

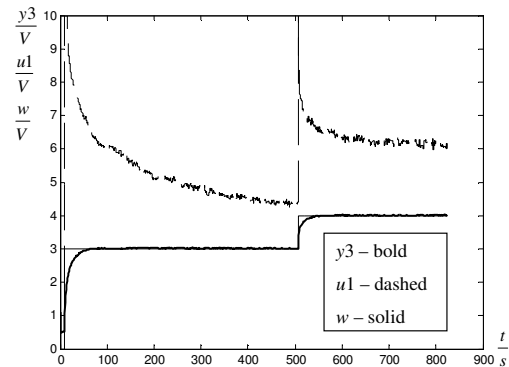


Figure 11: Control of Real Plant for D - K Iteration

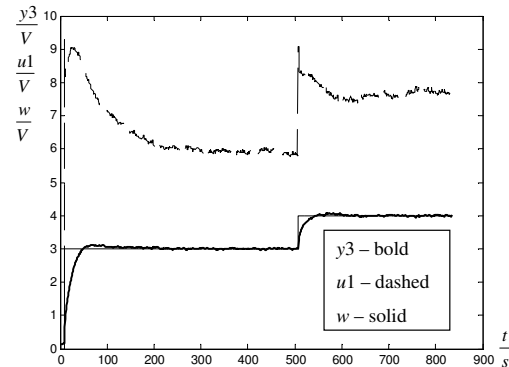


Figure 12: Control of Real Plant for Synthesis in R_{PS}

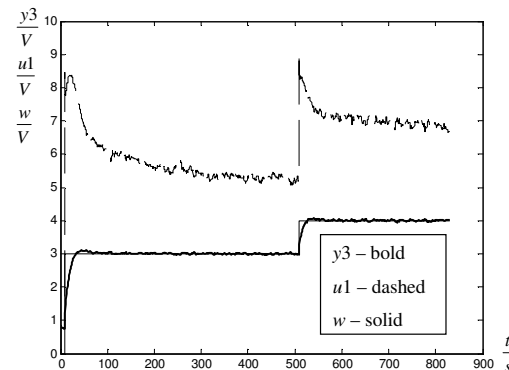


Figure 13: Control of Real Plant for Naslin Method

In order to provide a basis for comparison the controllers were tuned to give satisfactory overall performance across the complete temperature profile. The controllers designed in the ring of proper and stable functions (R_{PS} , see Prokop and Corriou 1997 or Prokop et al. 1992) and by the Naslin method were used as a reference (Figure 12 and 13). It is clear from Figure 9, 10, 11, 12, and 13 showing the system response and control input that the algebraic approach produces more favourable results. An improved accuracy in set-point tracking as well as lower energy consumption of the algebraic μ -synthesis (Figure 10) was achieved via increased control effort to the system resulting in higher variance in the control signal. The set-point, actuator and measured signals are in the unified voltage 0-10V of the CTRL unit. Performance indices are given in Table 2.

Table 2: Comparison of Performance Indices

Method	ϵ_1	ϵ_2	ϵ_3
Algebraic μ -synthesis	6.30	0.24	8.33
D - K iteration	6.37	0.23	9.07
R_{PS}	7.72	0.17	13.42
Naslin method	7.10	0.22	11.02

6. CONCLUSION

The contribution presents an application of the algebraic μ -synthesis to an air-heating set, where the temperature of bulb was controlled by its voltage. The controlled system had a nonlinear behaviour in both the steady-state and dynamic characteristics. The nonlinearity was treated via parametric uncertainty, which was transformed to the LFT framework. In order to achieve asymptotic tracking, performance weighting function with pole at the imaginary axis was used. The instability of the nominal feedback loop was treated by setting its poles to the left half-plane via pole placement technique and by choosing the PI structure of the controller which treats the unstable pole of the general closed-loop interconnection. The algebraic μ -synthesis was applied to the LFT interconnection including performance weight with integrating behaviour and the results were compared with standard methods for robust controller design - the D - K iteration, synthesis in R_{PS} and the Naslin method. Finally, it was shown that the algebraic μ -synthesis had better frequency properties in terms of μ -function and faster set-point tracking than the reference methods.

The algebraic μ -synthesis provides exploitable benefits for a wide range of industrial applications. In contrast to the D - K iteration, it can tune simple controllers in a more natural way and guarantee asymptotic tracking, which is desirable in most of the control tasks emerging in technology processes. The only drawback is the fact that an algorithm of global optimization is used leading to longer computational times.

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